

6/24/2020 Revisions – See page 2

Errata Sheet

PPI Handbook of Polyethylene Pipe, 2nd ed.

6/12/18

### **Chapter 8, Above-Ground Applications for PE Pipe**

**P. 326**

Under Reference #9, change title as follows: Plastics Addition ~~Addition~~ **Additives** Handbook ...

### **Chapter 6, Design of PE Piping Systems**

**P. 200, Table 3-3**

Update the Note as follows: ... see ASTM ~~F7906~~ **A796**. Based ..

3/22/2018

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**Chapter 6, Design of PE Piping**

Systems P. 158

$F_T$  = **Average Annual** Service Temperature Design Factor ...

**Chapter 3, Material Properties**

**P. 96: A.2- Values for Other Temperatures**

3rd - 4th lines: ... an **average annual** operating temperature (see **References at the end of this Appendix**) above the base temperature of 73°F (23°C) **typically** results in a decrease ...

5th line: Conversely, an **average annual** operating temperature below the base

8th-9th line: ... compensating factor for **average annual** operating temperatures ~~that ... 100°F (38°C)~~ **140°F are shown in Table A.2.** 10th line: delete full Paragraph ~~While the effect ... application under consideration.~~

**P. 97: Table A.2**

Table A.2 title: Change title to: **PE4710 Temperature Compensating Multipliers,  $F_T$**  Replace Table A.2 (and its 3 footnotes) with the following

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Design Temperature <sup>1</sup> Average Annual Operating- Temperature	Temperature <sup>2</sup> Compensation Multiplier, $F_T$
≤ 80°F (≤ 27°C)	1.0
> 80°F - 90°F (>27°C - 32°C)	0.9
> 90°F - 100°F (>32°C - 38°C)	0.8
> 100°F - 110°F (>38°C - 43°C)	0.8
> 110°F - 120°F (>43°C - 49°C)	0.7
> 120°F - 130°F (>49°C - 54°C)	0.7
> 130°F - 140°F (>54°C - 60°C)	0.6

<sup>1</sup> ~~The average annual temperature is a weighted average of the daily operating temperature, and is not the highest temperature observed in the system.~~

<sup>1</sup> The design temperature is the expected steady-state operating temperature of the pipe. For some applications, the design temperature may be the Average Annual Temperature (AAT). The AAT is based on the annual seasonal temperature fluctuations a buried piping system may be exposed to over the course of a year. Above ground pipelines require additional engineering considerations. For applications with significant operating temperature fluctuation or if the maximum HDB temperature is occasionally exceeded, refer to applicable codes and standards (e.g. ASME NM.1, etc.) or contact the pipe manufacturer for guidance.

<sup>2</sup> The  $F_T$  values are based on PE 4710 compounds with HDB = 1600 psi at 73°F and HDB = 1000 psi at 140°F and are calculated using the temperature equation that is shown in the PPI Handbook, Chapter 3, Appendix A and in PPI TR-3. HDB values are listed in PPI TR-4. Contact the manufacturer for other HDB and other  $F_T$  values. The  $F_T$  values shown in here are conservative since they are based on the highest temperature within each temperature range and are rounded.

**P. 98**

2nd line: change  $F_i$  to  $F_T$

3rd bullet: .. For example, AWWA standards C 901 and C906 and manual M55 which covers PE pressure class (PC) pipe already includes an similar abbreviated table of temperature compensating multipliers that differ slightly from what is presented in here.

Add at the end of Appendix A, Chp. 3: References on the use of Average Temperatures

**IGN 4-32-18** (2003), The Choice of Pressure Ratings for Polyethylene Pipe Systems for Water Supply and Sewerage Duties- UK Water Industry Information & Guidance Note- See section 4.2.2.1 titled Average Operating Temperature.

**Gran-Meyer, E.** (2005), Polyethylene Pipes in Applied Engineering, Total Petrochemicals, Belgium- See Sec. 11.04.1 (p. 481) titled Operation - Service Life

**Palermo, G., Zhou, J. and Farnum, R.** (2007), Effect of Elevated Ground Temperature (from Electric Cables) on the Pressure Rating of PE Pipe in Gas Piping Applications, AGA Operations Conference, Grapevine, TX

**CAN/CSA- Z662** (2011), Oil and Gas Pipeline Systems, Standards Council of Canada, See Sec. 12.4.2.5 (p. 259)

**Wedgner, A.** (2014), How to Design PE100 Pipes for Higher Operating Temperatures? Borouge Newsletter, BorPipe, Issue 33, p. 8-9.

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## Errata Sheet

PPI Handbook of Polyethylene Pipe, 2nd ed.

### Chapter 6, Design of PE Piping Systems

#### Page 217

The equation for calculating  $\Delta X/D_M$  uses the apparent modulus for the condition of a rapidly increasing stress or strain to solve for deflection due to only dead load; this calculation uses  $E = 130,000$  psi per as shown in Table B2.1, p. 101. Instead, use  $E$  from Chp. 3, p. 99, Table B.1.1; for example, for PE 4710 and a load duration of 100 years,  $E = 28,000$  psi. Also, under SOLUTION above the equation for  $\Delta X/DM$ , change '130,000' to "28,000" and change 'B2.1' to "B1.1".

#### Page 229

Under '(From Equation 3-23)' change "0.57" to 0.56" to match the answer shown above in the equation for VAF

#### Page 236, Table 3-14

Change the heading of the 2<sup>nd</sup> column from "Saturated, unit weight of ground water, pcf" to "Saturated Unit Weight of Soil, pcf". Keep the current symbol  $w_s$  as shown.

Change the heading in the 3<sup>rd</sup> column from "Dry, the weight of saturated soil above the pipe, lbs per foot of pipe" to 'Dry Unit Weight of Soil, pcf'. Keep the shown symbol  $w_d$  as shown.

#### Page 261, Appendix A.3

The definition of the variable C (Hazen-Williams Friction Factor ...) incorrectly refers the reader to see table 1-7. Change 'table 1-7' to "definitions below equation 2-12, p. 175"

#### Page 336 (3/4/16)

##### Under Mechanical Compression

change 4<sup>th</sup> sentence as follows: It is important that the ~~inside of the pipe wall .... avoid deflection of the pipe~~ use of stiffener to support the pipe wall may be required – refer to the manufacturer's instructions for specific detail on stiffener requirements.

## Chapter 7, Underground Installation of PE Piping

### p. 292, Table 4

Change title of Table to 'Minimum **Long-Term** Bend Radius for PE Pipe Installed in Open Cut Trench'

Change the heading of 1st column to "Dimension Ratio-DR"

## Chapter 8, Above-Ground Applications for PE Pipe

**Page 318** Equation 6 is applicable where support spacing is relatively large and the spacing and support rigidity do not induce axial compression in the pipeline in response to changes in temperature.

**Page 320** Equation 8 is applicable only when thermal expansion of the supported pipeline is not anticipated.

**Page 322/323** Equation 11 and 13 are applicable where support spacing and support rigidity do not induce axial compression in the pipeline in response to changes in temperature.

**Note:** Where spans between support spacing are relatively short and the span length and support rigidity induce axial compression in the pipeline in response to changes in temperature, the reader is referred to 'Roark's Formulas for Stress & Strain' by Warren C. Young, Table 10, Page 166.

## Chapter 10, Marine Installations

**P. 379** Change title of table to: Table 3 ~~Pipe Diameter Multipliers for the Determining of~~ Minimum **Short-Term** Bending Radius'

**Page 363, Step 3:** Add this new Paragraph under the heading of Step 3: General: Calculation of 'maximum weighting' (Step 3b) and calculations to determine the percent air entrapment that may cause the pipe to refloat (Step 3d) are based on the selected DR. Calculations to determine the recommended weighting (Step 3c) is based on achieving a weighting that is 'equivalent' to the weight of the water displaced by the pipe and is independent of DR. Other marine installation handbooks include calculations to determine the recommended weighting that are dependent on DR. Contact the pipe manufacturer or contractors experienced in this field for additional advice.

**Page 363, Step 3a:** Change the title of this section to "Buoyant Force as a Percentage of Air Inside the Pipe."

**Page 364, Step 3a:** Add the following text to the end of Step 3a: “In a pond or otherwise under conditions of no current, the minimum weight required to anchor the pipe equals the buoyant force times a safety factor. The weight of individual anchors may be found by multiplying the safety factored buoyant force (per unit length) times the anchor spacing.”

**Page 365, Step 3b:** Change the title of this section to “Practical Limit of Individual Ballast Weight (in air) for Towing of 100% Air Filled Pipe”

**Page 365, Step 3c:** Add the following as the first sentence in this section: The methodology described in this section is for pipelines that remain full of water, such as pressurized water lines. If you put in a line that contains primarily air, the weighting factors will not be conservative and may not be sufficient to prevent flotation.

**Page 367, step 3d:** The ratio of the selected ballast weight (Step 3c) divided by the minimum ballast weight to offset anticipated % air (Step 3a) may be regarded as the Factor of Safety against refloating the pipe. This may provide some safety factor against air entrapment but at the cost of reducing the safety factor against current moving the line.

**Page 392-393; Table A-3-1 and Table A-3-2** Add this text before Table A-3-1:

The ballast physical dimensions, ballast weights, and ballast spacing shown in tables A-3-1 and A-3-2 are approximate and are often significantly different than when calculated from first principles.

The reader is advised to calculate the volumes of anchor blocks from first principles and to determine weights based on the densities for ‘plain’ and ‘reinforced’ concrete shown on page 369. As there is often a discrepancy between the ‘produced’ weight of the anchor block versus the theoretical weight, the reader is referred to Section 3e for advice about adjusting the ballast spacing to achieve the desired ‘weighting percentage’.

The Tables assume the pipelines remain full of water, such as pressurized water lines. If you put in a line that contains primarily air, the weighting factors will not be conservative and may not be sufficient to prevent flotation.

**Chapter 12, Horizontal Directional Drilling**

**P. 435**

**TABLE 1**

Safe Pull Tensile Stress @ 73°F

Proposed Table 1				
Typical Safe Pull Stress (psi) @ 73°F				Time under tension design factor per ASTM F1804, note 4
PE 2xxx	PE 3608	PE 4710		
ASTM D3350 Cell Classification	PE234373	PE345464	PE445574	
Minimum Tensile yield strength (psi) per ASTM D3350	2600	3000	3500	
Tensile yield design factor per ASTM F1804	0.4	0.4	0.4	
Duration (hours)				
0.5	1040 <span style="background-color: yellow;">(use 1050)</span>	1200	1400	1.0
1	1040 <span style="background-color: yellow;">(use 1050)</span>	1200	1400	1.0
12 <small>(also used in PPI BoreAid and Calculator)</small>	988 <span style="background-color: yellow;">(use 1000)</span>	1140 <span style="background-color: yellow;">(use 1150)</span>	1330 <span style="background-color: yellow;">(use 1300)</span>	0.95
24	946 <span style="background-color: yellow;">(use 950)</span>	1092 <span style="background-color: yellow;">(use 1100)</span>	1274 <span style="background-color: yellow;">(use 1250)</span>	0.91

**P. 423, Pilot Hole Reaming** add the text in red: Normal-oversizing may be from 1.2 to 1.5 times the diameter of the carrier pipe, **but at least 4" larger than the diameter of the carrier pipe.**

**Index** The page numbers that are being referred to in the Index do not match the text. Reader is encouraged to use the search engine on the PPI website at <http://plasticpipe.org/search.html>